

On page 24, starting at line 13, please delete [[(cf. for example table)]], and add (see for example the foregoing table).

IN THE CLAIMS:

Please amend the claims as follows, without prejudice.

1. (Currently Amended) A method for the production of shaped zeolites, characterized by the process steps of:

a) mixing of (i) at least one type of zeolite crystal from the faujasite family having an  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio of  $\leq 3.0$ , ~~in particular zeolite LSX or zeolite LSX and zeolite 13X, with~~ (ii) finely divided attapulgite binder, or finely divided attapulgite binder and at least one further clay binder, the finely divided attapulgite binder being characterized in that its bulk density, measured according to EN ISO 797:1995D, is greater than 550 g/l, and (iii) [[addition of]] water,

b) [[production of]] producing shaped zeolite bodies from the mixture prepared in step a),

c) drying and [[calcination]] calcinating of the zeolite bodies shaped in step [[a]] b) in order to obtain [[the]] an active adsorbent[[,]].

~~the finely divided attapulgite binder being characterized in that its bulk density, measured according to EN ISO 797:1995D, is greater than 550 g/l.~~

2. (Currently Amended) The [[process]] method as claimed in Claim 1, characterized in that an ion exchange is effected after step c).

3. (Currently Amended) The method as claimed in Claim 1 [[or 2]], characterized in that the proportion of the binder in the finished adsorbent accounts for a proportion of between 2 and 30 percent by weight.

4. (Original) The method as claimed in Claim 3, characterized in that the proportion of the binder in the finished adsorbent accounts for a proportion of between 5 and 20 percent by weight.

5. (Currently Amended) The method as claimed in [[any of the preceding claims]] Claim 1, characterized in that not more than 10 to 90% of the binder is conventional clay binder.

6. (Original) The method as claimed in Claim 5, characterized in that not more than 80% of the binder is conventional clay binder.

7. (Original) The method as claimed in Claim 5, characterized in that not more than 70% of the binder is conventional clay binder.

8. (New) The method of Claim 1, wherein the at least one type of zeolite crystal from the faujasite family having an  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio of  $\leq 3.0$  is selected from the group consisting of zeolite LSX and zeolite 13X.

[[8]] 9. (Currently Amended) The method as claimed in [[any of the preceding claims]] Claim 8, characterized in that the zeolite types 13X and LSX are used in a ratio of from 90:10 to 5:95.

[[9]] 10. (Currently Amended) The method as claimed in Claim 8 [[any of the preceding claims]], characterized in that at least 70%[, preferably at least 90%,] of the two zeolite types 13X and LSX are present in the sodium form.

11. (New) The method as claimed in Claim 8, characterized in that at least 90% of the two zeolite types 13X and LSX are present in the sodium form.

[[10]] 12. (Currently Amended) The method as claimed in Claim [[9]] 8, characterized in that not more than 30%[, preferably not more than 10%,] of the two zeolite types 13X and LSX are present in the potassium form.

13. (New) The method as claimed in Claim 8, characterized in that not more than 10% of the two zeolite types 13X and LSX are present in the potassium form.

[[11]] 14. (Currently Amended) The method as claimed in [[any of claims 1 to]] Claim 8, characterized in that from 60 to 95%[, preferably between 75 and 85%,] of the two zeolite types 13X and LSX are present in the calcium form.

15. (New) The method as claimed in Claim 8, characterized in that between 75 and 85% of the two zeolite types 13X and LSX are present in the calcium form.

[[12]] 16. (Currently Amended) The method as claimed in [[any of the preceding claims]] Claim 1, characterized in that a pore-forming agent is added to the mixture of the zeolite crystals and the binder.

[[13]] 17. (Currently Amended) The method as claimed in [[any of the preceding claims]] Claim 16, characterized in that the pore-forming agent is added in an amount which corresponds to an amount between 2 and 15 percent by weight, based on the finished product.

[[14]] 18. (Currently Amended) A zeolitic adsorbent obtainable by means of the method as claimed in [[any of the preceding claims]] Claim 1.

[[15]] 19. (Currently Amended) A method for eliminating one or more impurities from a gas stream, characterized in that the gas stream is passed through a bed of the zeolitic adsorbent as claimed in Claim [[14]] 18.

[[16]] 20. (Currently Amended) The method as claimed in Claim [[15]] 19, characterized in that the gas stream is an air stream and the impurity is selected from the group consisting of carbon dioxide, water, nitrous oxide, another inorganic gas, hydrocarbons and mixtures of two or more of these substances.

[[17]] 21. (Currently Amended) The method as claimed in Claim [[15 or 16]] 19, characterized in that the impurity is carbon dioxide.

[[18]] 22. (Currently Amended) The method as claimed in [[any of Claims 15 to 17]] Claim 21, characterized in that the [[adsorption]] eliminating one or more impurities is effected alternately with a desorption in the PSA mode or in particular in the TSA mode.

23. (New) The method as claimed in Claim 21, wherein in that the eliminating one or more impurities is effected alternately with a desorption in the TSA mode.